AMENDMENTS TO THE CLAIMS

1. (Currently amended) A process in gaseous phase to obtain CFC 113a starting from CFC 113, wherein CFC 113, optionally diluted with a gas inert under reaction conditions, is let flow on a catalyst consisting of aluminum fluoride in a fixed or fluidized bed at a reaction temperature of from 50°C to **280 °C** ~~less than 200°C~~ **wherein the content of residual CFC-113 in the obtained CFC-113a in the final reaction mixture is lower than 1% by weight based on CFC-113a and CFC-113 present in the mixture**.

2. (Original) A process according to claim 1, wherein CFC 113 is used in admixture with CFC 113a.

3. (Previously presented) A process according to claim 1, wherein the fed CFC 113 amount, expressed as weight ratio between CFC 113/(catalyst x hour), is in the range 0.5-1.5.

4. (Currently amended) A process according to claim 1, wherein the aluminum fluoride is obtained by ~~fluorination of~~ **fluorinating an** aluminum oxide with anhydrous hydrogen fluoride so that the introduced fluorine amount corresponds to 95% by weight or more.

5. (Previously presented) A process according to claim 4, wherein the reaction temperature is at least 100°C.

6. (Previously presented) A process according to claim 5, wherein the reaction temperature is in the range of 100°C - 160°C.

7. cancelled

8. (Currently amended) A process in gaseous phase to obtain CFC 113a from CFC 113, wherein CFC 113, optionally diluted with a gas inert under reaction conditions, is let flow on a catalyst consisting of aluminum fluoride in a fixed or fluidized bed at a reaction temperature of from 50°C to ~~about~~ 183°C, wherein the content of CFC-113a in the **final** reaction mixture is ~~at least~~ 77.73% **to 84.73%** by weight.

9. (previously presented) A process according to claim 8, wherein CFC 113 is used in admixture with CFC 113a.

10. (previously presented) A process according to claim 8, wherein the fed CFC 113 amount, expressed as weight ratio between CFC 113/(catalyst x hour), is in the range 0.5-1.5.

11. (currently amended) A process according to claim 8, wherein the aluminum fluoride is obtained by ~~fluorination of~~ **fluorinating an** aluminum oxide with anhydrous hydrogen fluoride so that the introduced fluorine amount corresponds to 95% by weight or more.

12. (previously presented) A process according to claim 11, wherein the reaction temperature is at least 100°C.

13. (previously presented) A process according to claim 12, wherein the reaction temperature is in the range 100°C - 160°C.

14. (Currently amended) A process according to claim 8, wherein the content of residual **CFC-113 in the obtained CFC -113a** ~~CFC 113~~ in the **final** reaction mixture is lower than 1% by weight based on CFC-113a and CFC-113 present in the mixture.

15. (Currently amended) A process according to claim 8, wherein the content of ~~CFC-113a~~ **CFC-113** in the **final** reaction mixture is **from 0.35% by weight to** ~~at most~~ 0.97% by weight.

16. (Currently amended) A process in gaseous phase to obtain CFC 113a starting from CFC 113, wherein CFC 113, optionally diluted with a gas inert under reaction conditions, is let flow on a catalyst consisting of aluminum fluoride in a fixed or fluidized bed at a reaction temperature of from 100°C to 160°C, wherein the content of residual CFC-113 **in the obtained CFC-113a** in the **final** reaction mixture is less than or equal to 0.9% by weight based on CFC-113a and CFC-113 present in the mixture.

17. (previously presented) A process according to claim 16, wherein CFC 113 is used in admixture with CFC 113a.

18. (previously presented) A process according to claim 16, wherein the fed CFC 113 amount, expressed as weight ratio between CFC 113/(catalyst x hour), is in the range 0.5-1.5.

19. (currently amended) A process according to claim 16, wherein the aluminum fluoride is obtained ~~fluorination of~~ **fluorinating an** aluminum oxide with anhydrous hydrogen fluoride so that the introduced fluorine amount corresponds to 95% by weight or more.